


**IEEE PES Workshop
on Energy Systems
Simulation and
Modeling**

Turbine and Boiler Modeling
Impact on Generator's Performance

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**Why study Plant
Performance ?**



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Why study Plant Performance ?

Plant - System interaction law

$$J \frac{d\Omega}{dt} = C_m - C_e$$

Turbogenerator group rotational velocity → $d\Omega$
Turbogenerator group rotational inertia → J
Mechanical torque → C_m
Electrical load demand/torque → C_e

- Unbalance between power production and electrical consumption ⇒ frequency variation
- Objective : to control the grid frequency by acting on the mechanical torque

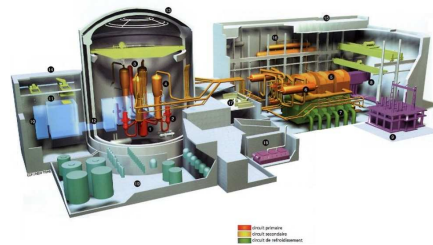
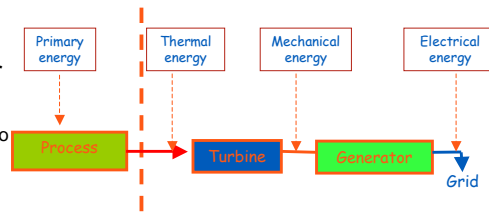
Two main issues:

- Electrical and mechanical variables have different dynamics → must be taken into account for control system design
- Turbine must be protected from system operation faults → may be handled using a global control loop

Why study Plant Performance ?

Two main categories of power plants:

- Electrical production can be adjusted to the grid demand
 - > Nuclear
 - > Fossil fuel
 - > Combined cycle
 - > Hydraulic
- Electrical production cannot be adjusted to the grid demand
 - > Renewable
 - > Distributed production ...

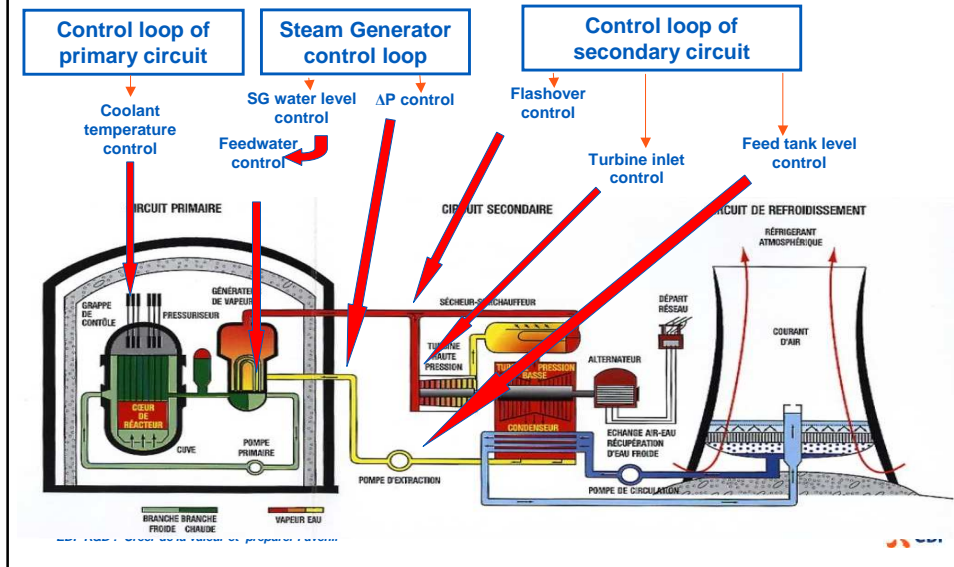


3D view of the EPR

⇒ various characteristics (constraints and benefits)

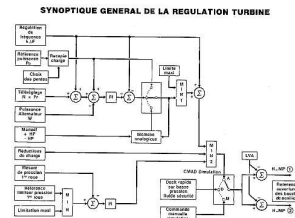
Nuclear – PWR

Global view of Nuclear Power Plant and its control loops



NPP

- ◆ Principle : At each instant time, the delivered electrical power is practically equal to the nuclear power (almost no energy storage)
- ◆ Primary coolant system (RCS)
 - Complex behavior : complex physics (radioactivity decay, xenon oscillations...)
 - With many operating constraints : fuel cycle, safety rules...
 - Two main control means : control rods, boron concentration
- ◆ Secondary coolant system : interface between RCS and grid
 - GRE : multiple functional control loop
 - Rotational speed turbine shaft control
 - Electrical power control
 - High pressure turbine stage control
 - Thresholds for safety control
 - Grid demand automatic adjustment



NPP operation constraints

◆ Power plant limitations to the grid demand

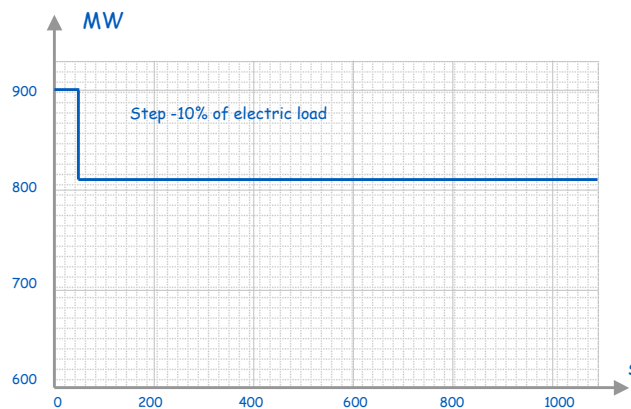
- Almost no energy reserve → grid load variation impacts directly the RCS (no damping between the two systems)
- Leads to frequent control rods movements

◆ Impact of grid operation faults on the NPP

- How to maintain the electrical supply to the auxiliaries ? Is the auxiliaries operation compatible with electrical perturbations ?
- What happens in case of islanding (rapid separation of the plant from the grid) ? In this case, how to rapidly evacuate the excess thermal power ?

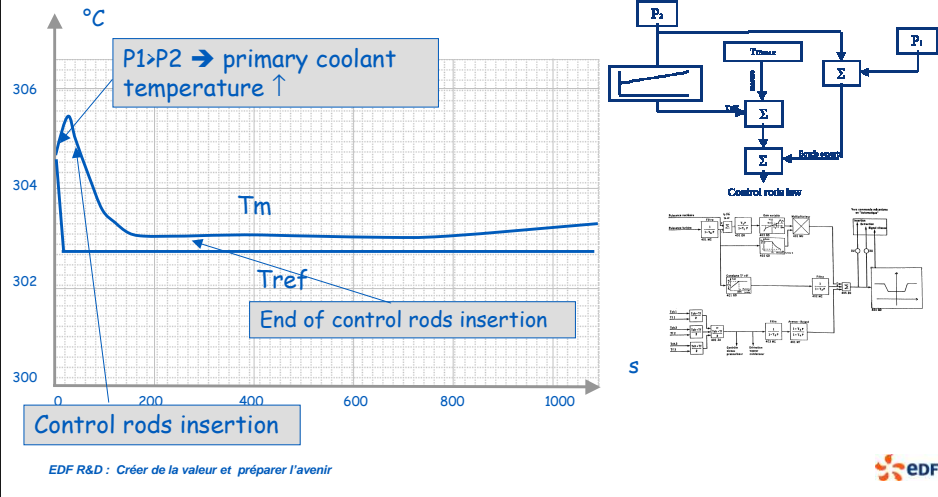
NPP: Electrical load step

◆ Electrical load:



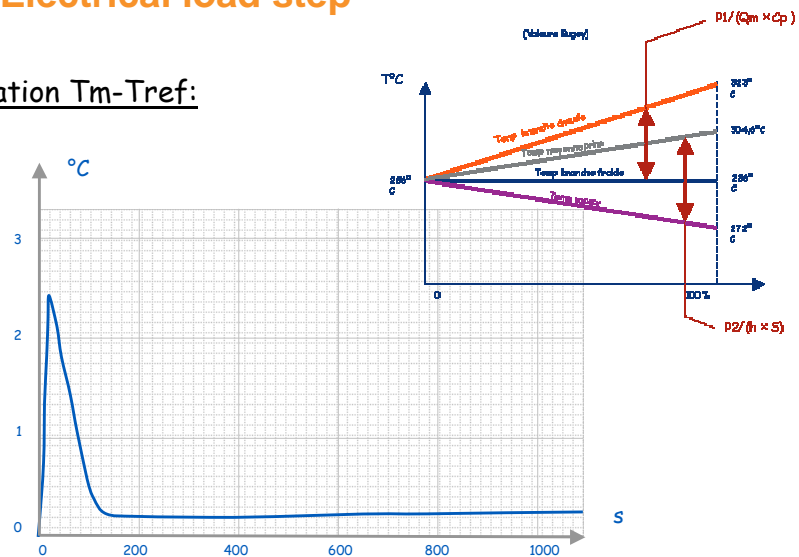
NPP: Electrical load step

◆ Primary coolant temperature:



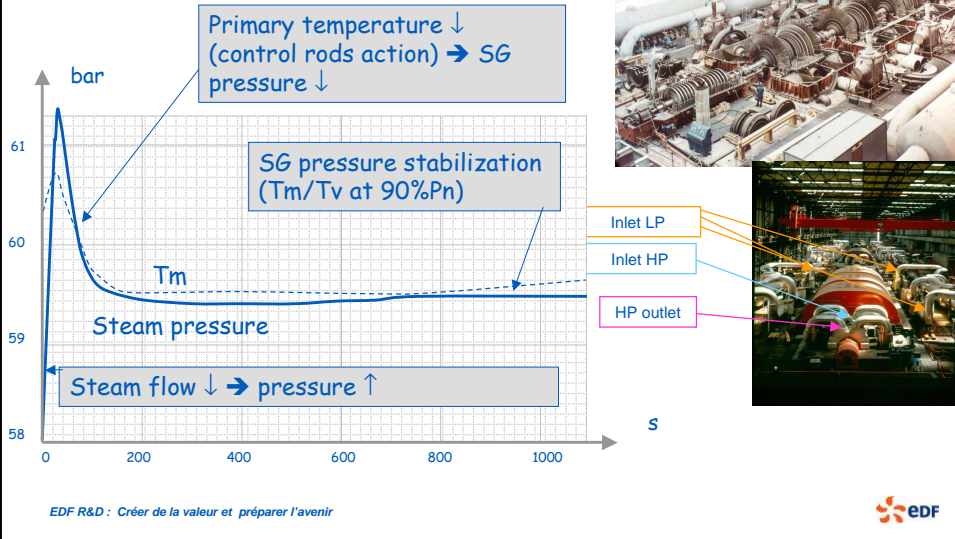
NPP: Electrical load step

◆ Deviation $T_m - T_{ref}$:



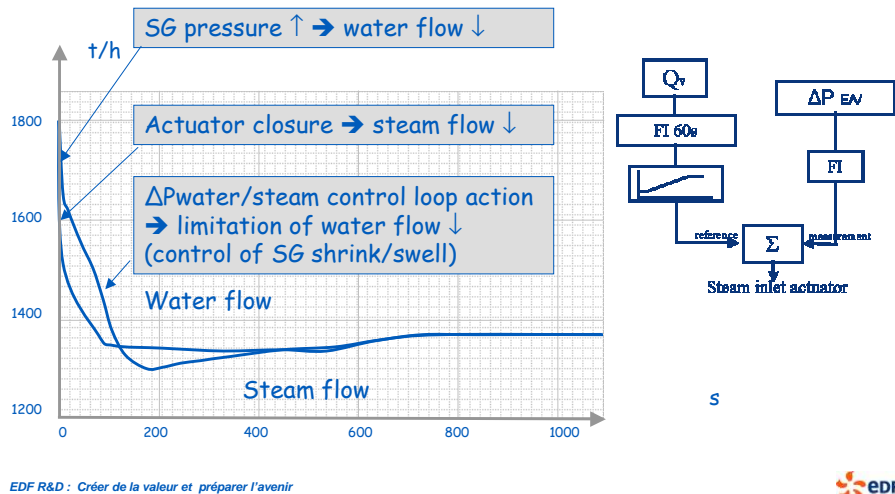
NPP: Electrical load step

Steam pressure:



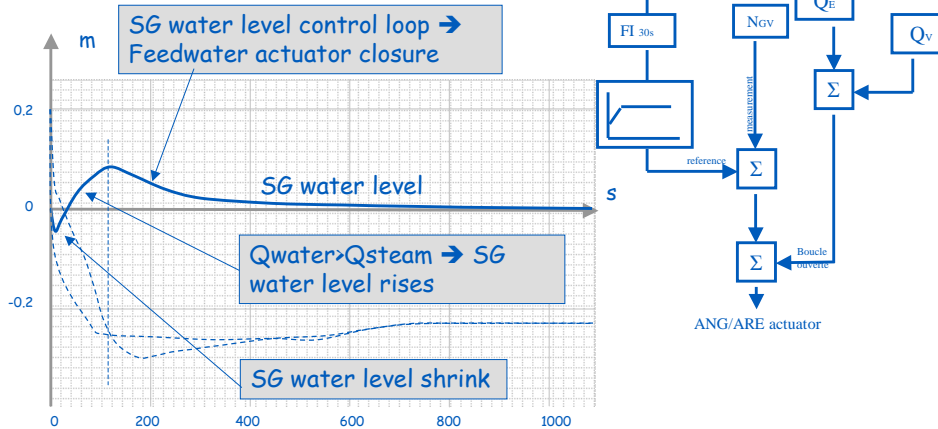
NPP: Electrical load step

Water - steam flows:



NPP: Electrical load step

SG water level:

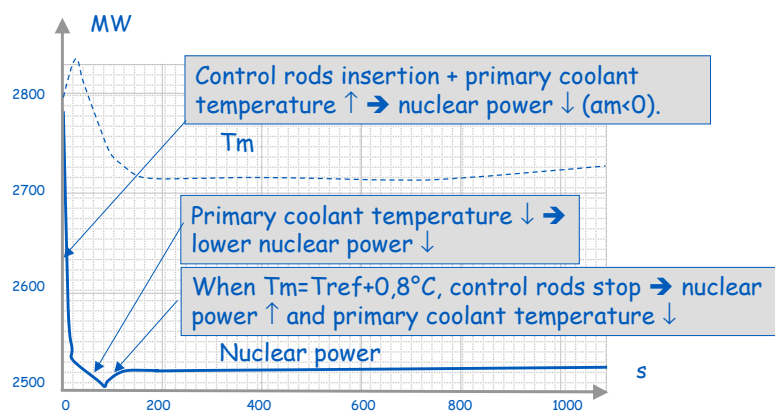


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NPP: Electrical load step

Nuclear power:

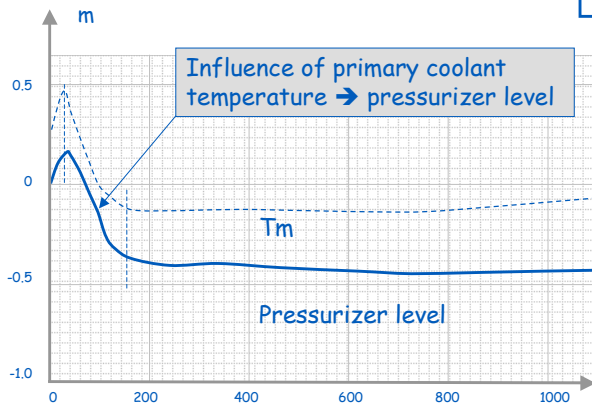


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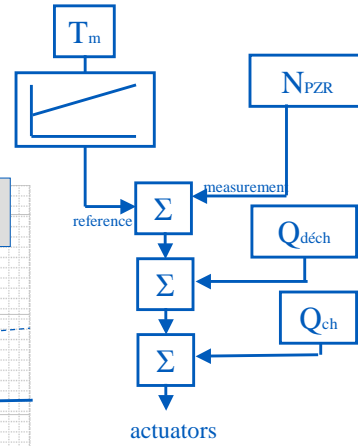


NPP: Electrical load step

◆ Pressurizer level:

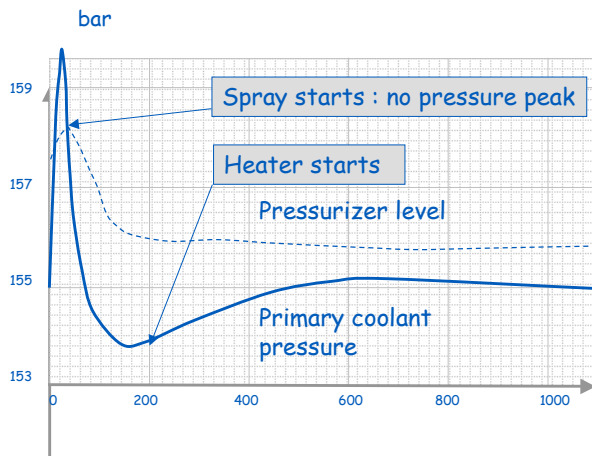


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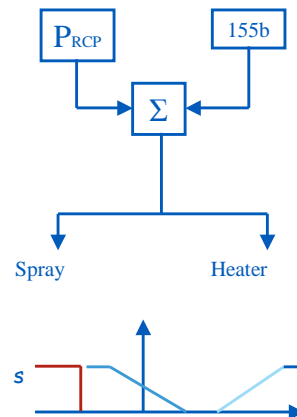


NPP: Electrical load step

◆ Primary coolant pressure:



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Fossil/conventional Power Plant

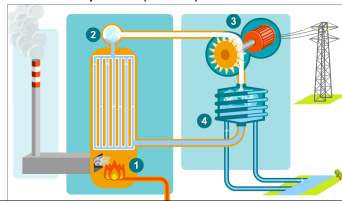
◆ Principle: load demand = boiler power production

◆ Boiler

- Different kinds: drum, once-through...
- Different fuels: coal, oil, gas...
 - Impact of coal grinding, oil preheating... on the plant dynamic behavior

◆ Operation constraints

- Grid demand
 - Better steam reserve compared to NPP (drums...): direct coupling between the drum boilers and the generator
- Grid operation faults
 - How to efficiently operate the plant auxiliaries: coal grinder, pumps... ?
 - How to rapidly evacuate the excess thermal power (steam) ?



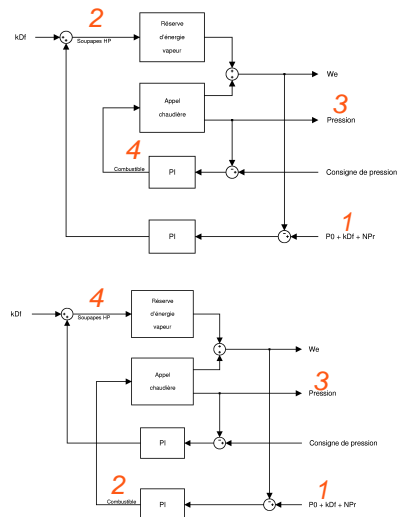
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Fossil/conventional Power Plant

◆ Two operating modes for drum boiler:

- Overriding turbine mode
- Overriding boiler mode

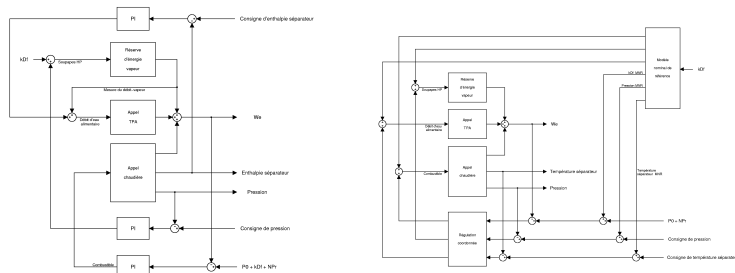


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Fossil/conventional Power Plant

- ◆ No drum = no steam reserve
 - ➔ Need of more efficient feedwater control strategy
- ◆ Advanced plant control strategy
 - Boiler-turbine coordinated control strategy : all actuators are directly controlled from the load variation
 - Some optimized anticipations with $k\Delta f$ variations (ancillary services)



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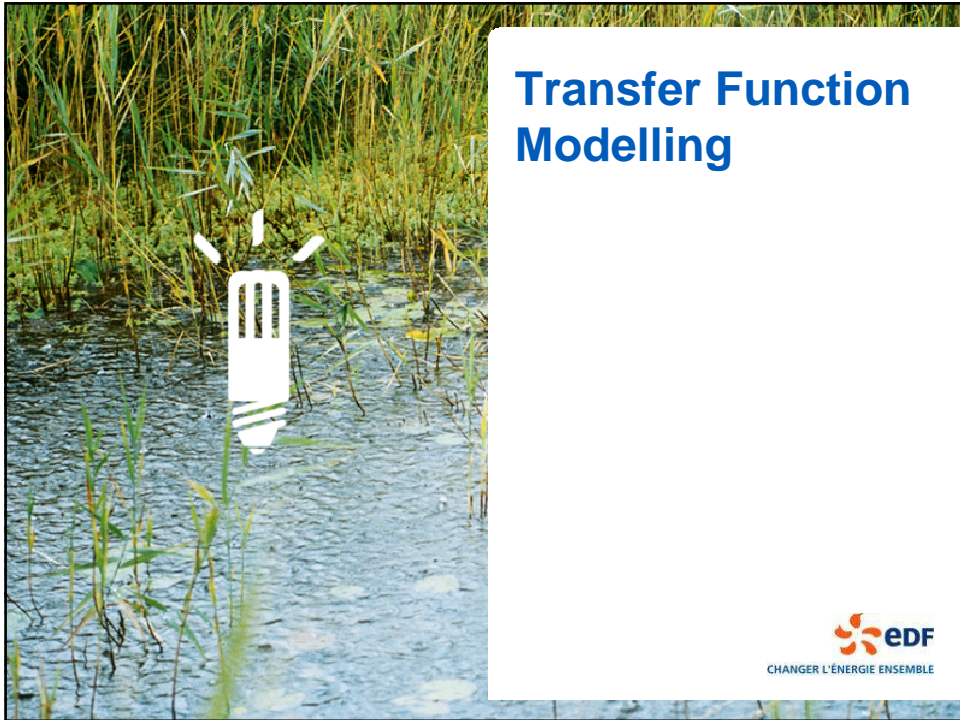


Why study Plant Performance ?

- ◆ Performances are heterogeneous depending on the plant type
 - Nuclear
 - Fossil fuel
 - Combined cycle
 - Hydraulic
 - ...
- ◆ But only one plant performance rule : UCTE (TSO) rules !
 - Regulation compliance for the plant dynamic behavior
 - Performance regulation are different for primary and secondary reserves

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Transfer Function Modelling



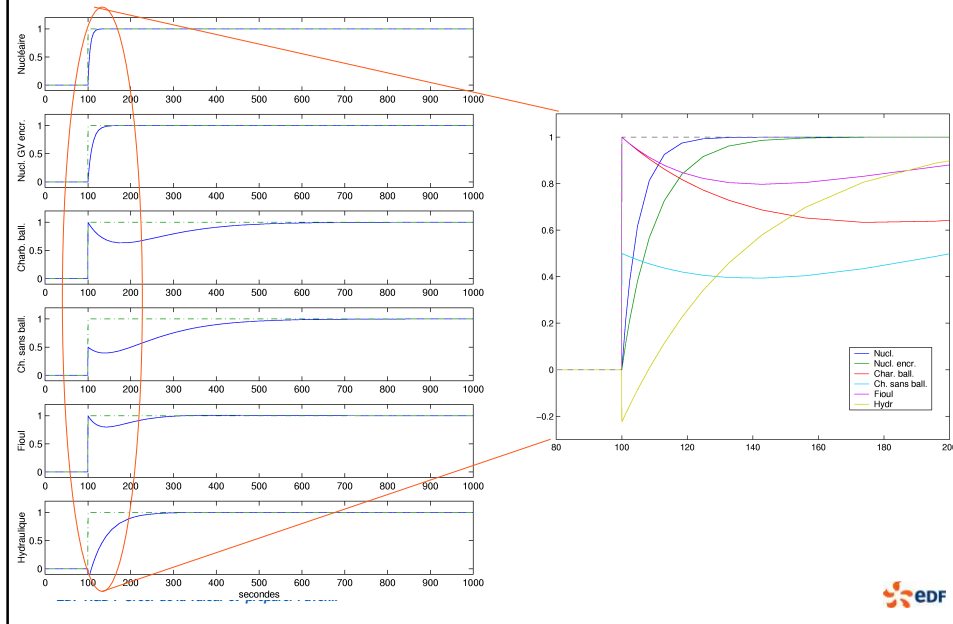
Power plant step response: primary reserve

Power plant	Frequency \rightarrow Load transfer functions
Optimal PWR	$\frac{1}{5s+1} \frac{1}{S_{nuc\acute{e}aire}} \frac{P_0}{f_0}$
Fouling SG PWR	$\frac{1}{10s+1} \frac{1}{S_{nuc\acute{e}aire}} \frac{P_0}{f_0}$
Drum equipped coal plant	$\frac{6400s^2 + 80s + 1}{6400s^2 + 160s + 1} \frac{1}{S_{charbon}} \frac{P_0}{f_0} \Delta f =$ $\left(\frac{80s}{80s+1} + \frac{1}{(80s+1)^2} \right) \frac{1}{S_{charbon}} \frac{P_0}{f_0} \Delta f$
No drum equipped coal plant	$\frac{3200s^2 + 40s + 1}{6400s^2 + 160s + 1} \frac{1}{S_{charbon}} \frac{P_0}{f_0} \Delta f =$ $\left(\frac{40s}{80s+1} + \frac{1}{(80s+1)^2} \right) \frac{1}{S_{charbon}} \frac{P_0}{f_0} \Delta f$
Oil plant	$\frac{200000s^3 + 8000s^2 + 160s + 1}{200000s^3 + 10500s^2 + 180s + 1} \frac{1}{S_{fioul}} \frac{P_0}{f_0} =$ $\left(\frac{80s}{80s+1} + \frac{1}{(50s+1)^2} \right) \frac{1}{S_{charbon}} \frac{P_0}{f_0} \Delta f$
Hydraulic plant	$\frac{-9s+1}{40s+1} \frac{1}{S_{hydraulique}} \frac{P_0}{f_0}$

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Power plant ramp response: primary reserve



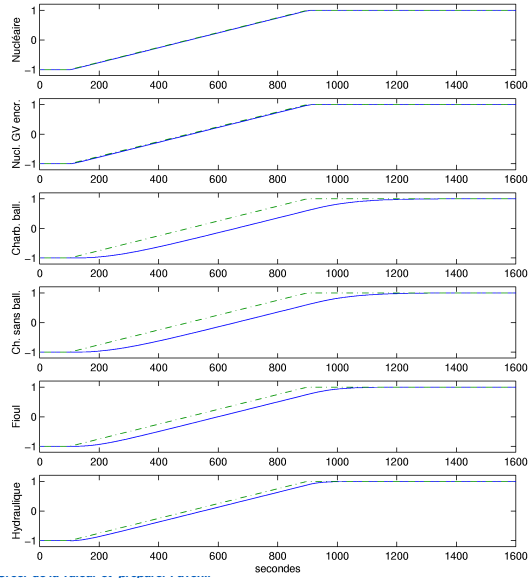
Power plant step response : secondary reserve

- ◆ The grid remote control signal is not directly applied to the high pressure valve actuators

Frequency → Load transfer

Power plant	functions
Optimal PWR	$\frac{1}{5s+1} P_r$
Fouling SG PWR	$\frac{1}{10s+1} P_r$
Coal plant	$\frac{1}{6400s^2 + 160s + 1} P_r = \frac{1}{(80s+1)^2} P_r$
Oil plant	$\frac{1}{2500s^2 + 100s + 1} P_r = \frac{1}{(50s+1)^2} P_r$
Hydraulic plant	$\frac{-9s+1}{40s+1} P_r$

Power plant ramp response: secondary reserve



EDF R&D :



MISTRAL models

◆ Simplified models (transfer functions) of plant dynamic behavior, developed:

- by R&D/STEP/P1B with Matlab/Simulink for the EDF fleet,
- for dynamic performance enhancement studies and new control design.

◆ A good trade-off between easy implementation and accurate physical representation

◆ Functional modular architecture:

- Physical process modules: major physical phenomena (non linear mass, momentum and energy conservation laws)
- Control loop modules : filters, thresholds, hysteresis...

◆ Validated with measurements data

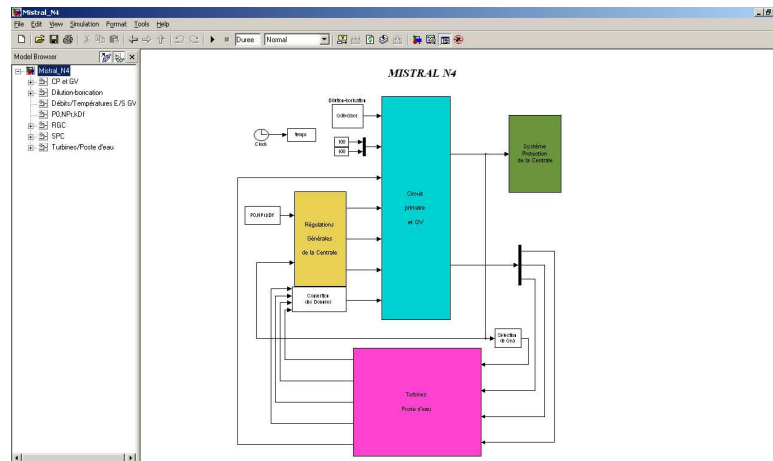
◆ Scope: steady state and normal transients

- Ancillary services, all kind of normal operation modes (upper than 20% Pn), major grid operation faults

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MISTRAL models

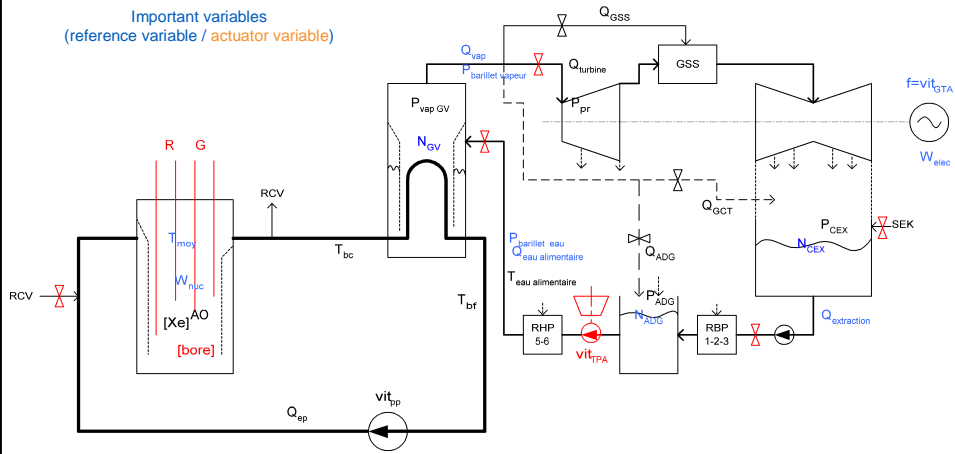


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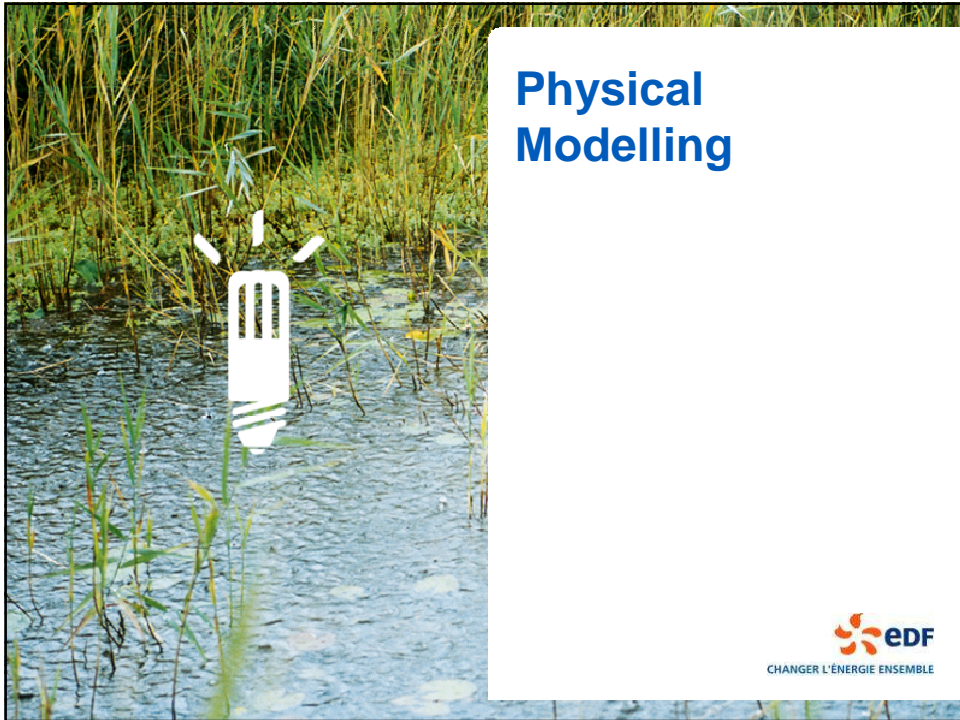


MISTRAL models

Important variables
(reference variable / actuator variable)



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Physical Modelling



Governing model equations

Equation	1D distributed formulation	Lumped formulation in model
Mass balance	$\frac{\partial(\rho_x \cdot A_x)}{\partial t} = - \frac{\partial(\rho_x \cdot v_x \cdot A_x)}{\partial x}$	$A \cdot \frac{d\rho_x}{dt} \cdot \Delta x = m_flow_x - m_flow_{x+\Delta x}$
Momentum balance	$\frac{\partial v_x}{\partial t} = - \frac{\partial}{\partial x} \left(\frac{v_x^2}{2} \right) - \frac{1}{\rho_x} \cdot \frac{\partial P_x}{\partial x} - g \cdot \frac{\partial z_x}{\partial x} - F_x$	$\frac{L}{A} \cdot \frac{d}{dt} m_flow_x \cdot \Delta x = \frac{m_flow_x^2}{A^2} \cdot \left(\frac{1}{\rho_x} - \frac{1}{\rho_{x+\Delta x}} \right) + P_x - P_{x+\Delta x} - F_x$ Staggered grid
Energy balance	$\frac{\partial}{\partial t} (\rho_x \cdot A_x \cdot u_x) = - \frac{\partial}{\partial x} (h_x \cdot \rho_x \cdot v_x \cdot A_x) + \pi \cdot D \cdot \phi_x$ $u_x = h_x - \frac{P_x}{\rho_x}$	$A \cdot \frac{d(\rho_x \cdot u_x)}{dt} \cdot \Delta x = h_x \cdot m_flow_x - h_{x+\Delta x} \cdot m_flow_{x+\Delta x} + \pi \cdot D \cdot \phi_x \cdot \Delta x$ $\phi_x = h_x \cdot (T_{w,x} - T_x)$

Homogenous model used for two-phase flow

GRETH correlations used to compute the friction and the heat transfer coefficient terms

IAPWS-IF97 polynomials used to compute the fluid physical properties

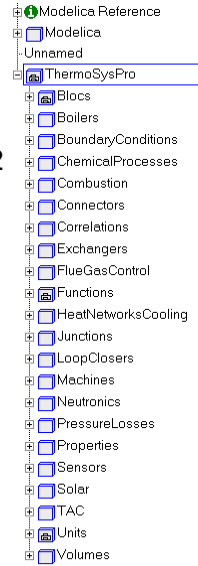
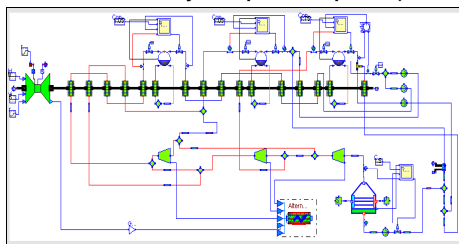
Physical modelling with the Modelica language

Modelica is a language for the modelling and simulation at the system level. Main benefits:

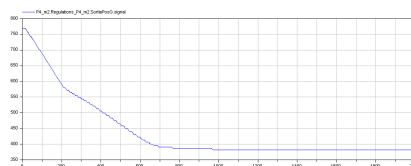
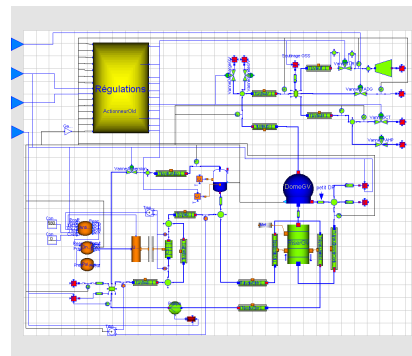
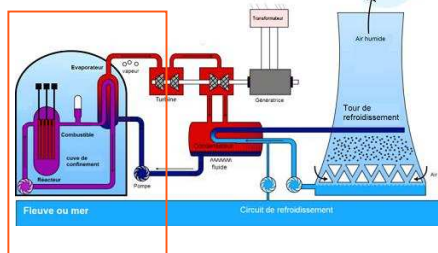
- 0D/1D
- Multi-domain: all branches of physics + control system
- Hybrid: handles continuous (e.g. thermofluid) and discrete (e.g. control logics) interacting parts
- Steady state/dynamic modelling
- A-causal: automatic model reversal (inverse problem solving)
- Declarative: optimized simulation code is automatically generated from the model equations
- Open source: developed and promoted by the Modelica Association
- Tool independent: language is supported by several commercial and open source tools (CATIA from DS, Scilab, OpenModelica...).

ThermoSysPro library

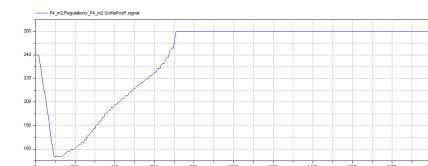
- ◆ Modelica library for static and dynamic power plant modelling
- ◆ Developed in the framework of the ITEA 2 EUROSYSLIB project
- ◆ Will be released as an open source library with two significant test-cases (concentrated solar power plant and combined cycle power plant)



Dynamic simulation of the islanding of the 1300 MWe NPP (P4)




G control rods position



R control rods position

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Modeling of Steam Generators of Nuclear Power Plants to assess TSP blockage Phenomena and Performance

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in collaboration with
 Vincent Chip (École Polytechnique)
 Aurélien Gay (École Polytechnique)



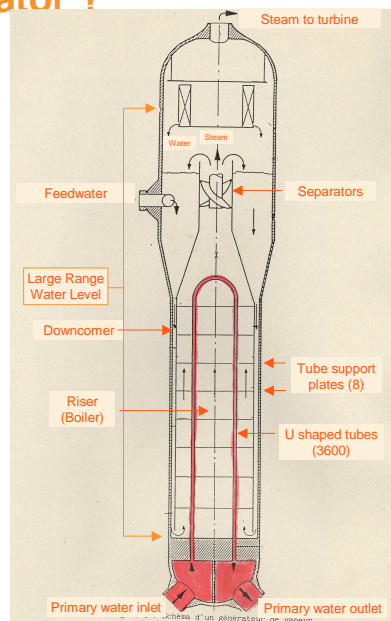
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What is a PWR steam generator ?

◆ Important component:

- Barrier between the primary and secondary loops : 2nd safety barrier
- Cool the fission reactor and produce steam for the turbine-generator
- Works as a complex counter-current and co-current flow heat exchanger

	Primary loop	Secondary
Temperature at inlet	322°C	220°C
Temperature at outlet	284°C	270°C
Mean pressure	155 bar	55 bar
Mass flow	15 900 t/h	1 800 t/h
Steam quality at outlet		99.75 %
Circulation ratio = total flow / steam flow		Between 4 and 5



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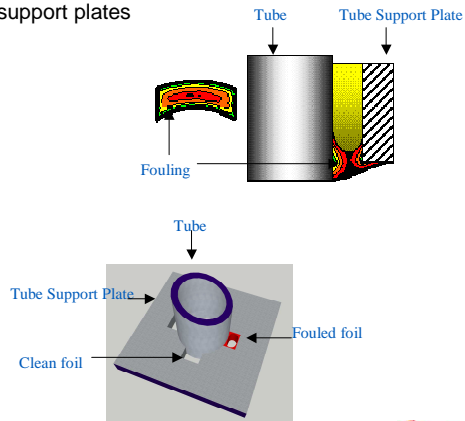
What is the TSP blockage phenomena and its consequence ?

Deposits of iron oxide particles:

- On the U-tubes outer walls
 - ↳ Impacts the heat exchange capacity
- On the quatrefoil sections of the U-tubes support plates
 - ↳ Reduces the flow rate through the sections

Problem:

- Reduce cooling efficiency
- May lead to safety issues



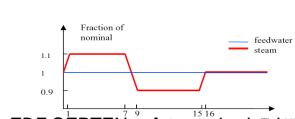
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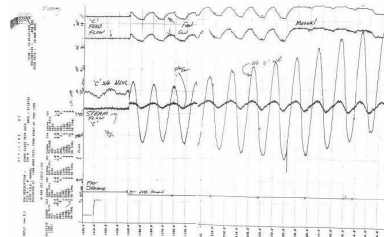
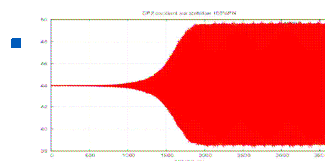
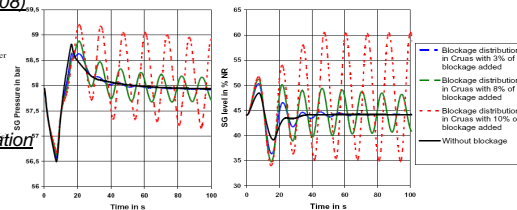
What is the TSP blockage phenomena and its consequence ?

Impact on SG behavior during transient: oscillation of water level

- IRSN article (ICONE 16 – May 2008)



- EDF-SEPTEN safety study simulation



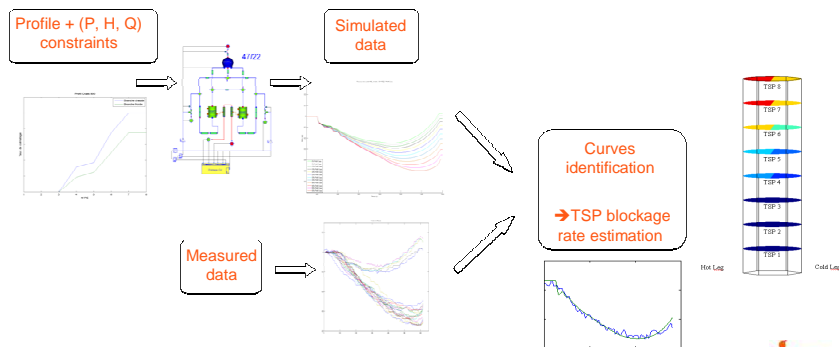
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New method to assess TSP blockage

Proposed new method

- Based on the analysis of the response of the SG to a particular transient: the periodic testing of the control rods that leads to a 60% power derate in 20 minutes (EP RGL 4)
- Can be performed between two yearly outages (in comparison with local inspections such as eddy current measurements or camera inspections)
- Produces a global estimator (instead of local estimators)



SG model: Modelica model

U-shaped tubes:

- One equivalent distributed pipe
- Heat transfer (Dittus-Boelter)

Riser:

- Dissymmetry between hot and cold leg
- Each leg modelled as a distributed pipe
- Friction coef. to represent the singular pressure losses due to blockage (Chisholm 1983)
- Heat transfer from U-tubes (Jens&Lottes)
- Two-phase flow model (Chisholm 1973)

Downcomer:

- Each leg modelled as one simple adiabatic pipe to represent the effect of gravity

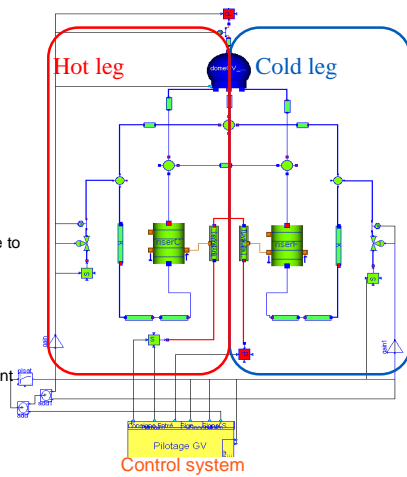
Separators:

- Pressure losses (simple pipes)
- Two-phase cavity

Control system:

- Water level control
- Follow-up of primary mass flow temporal profile during EP RGL4 transient

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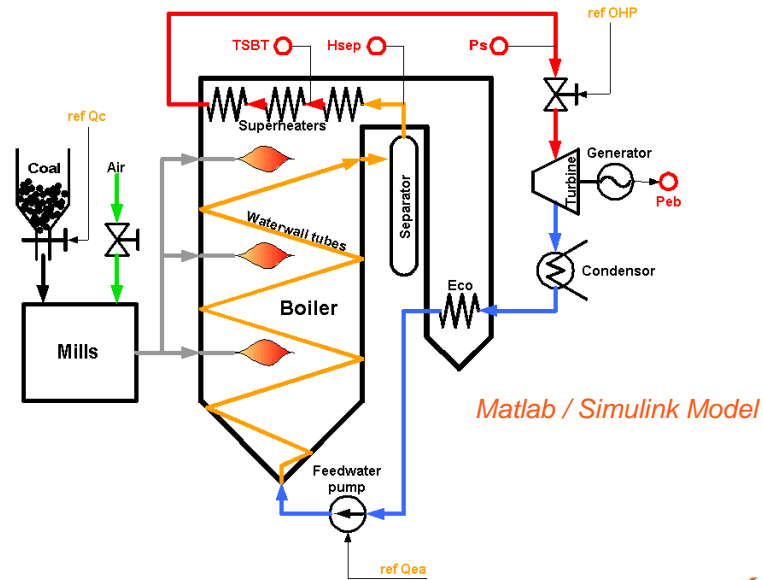
Results and conclusion

- ◆ It is possible to compute a global estimator of the TSP blockage rate. This indicator is very useful for the planning of the yearly maintenance operations.
- ◆ This global estimator is obtained using a dynamic model of the SG written in the object-oriented Modelica language.
- ◆ It is important to know how PWR components are for ancillary services : reserves must be available at any time

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Q600 coal power plant

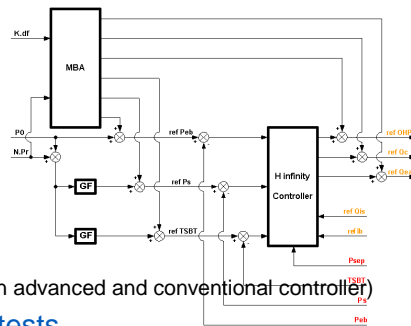


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Advanced control methodology

- ◆ On-site open loop tests
 - PI in manual mode
 - Steps applied to the process (actuators)
- ◆ Modelling, identification algorithms
- ◆ Design
 - Advanced controller synthesis (H^∞ controller)
 - Simulation in closed loop (comparisons between advanced and conventional controller)
- ◆ Implementation & on-site validation tests



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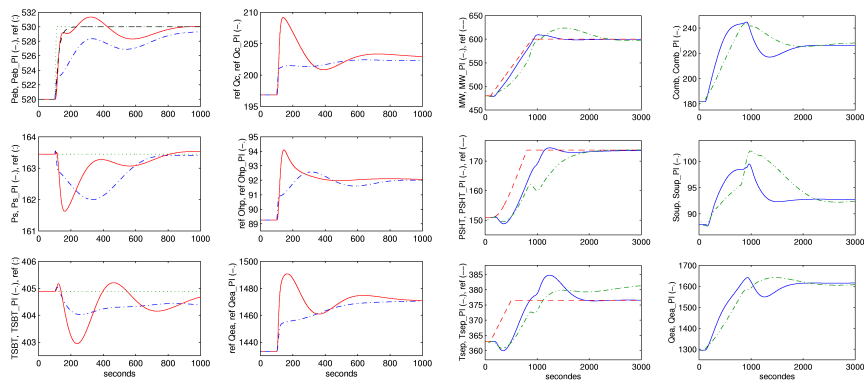


Advanced controller for ancillary services

■ Primary criteria

■ Secondary criteria

Response simulation

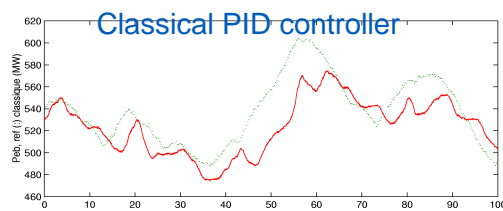
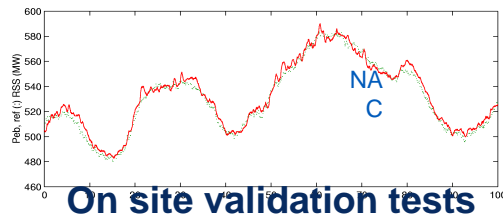


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Advanced controller for ancillary services

► Load follow-up under normal operation: $ref\ Peb = P_0 + K.\Delta f + N.Pr$



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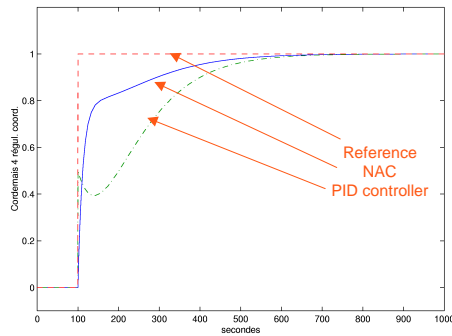


Advanced controller for ancillary services

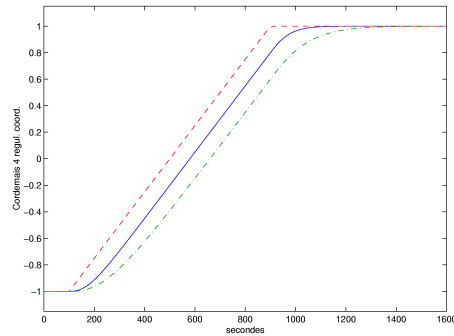
► The Model Base Anticipation (MBA) added value

- Open-loop anticipation on Actuators and References

→ Enhancement of dynamic performance must be taken into account for system



Primary reserve



Secondary reserve

EDF R&D : Créer de la valeur et préparer l'avenir

